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Effect of *Santolina pectinata* (Lag.) Essential Oil to protect against the corrosion of Mild steel in 1.0 M HCl: Experimental and quantum chemical studies

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Abstract: The essential oil of *Santolina pectinata* aerial parts (SP oil) was extracted by hydrodistillation and analyzed by Gas Chromatography (GC) and Gas Chromatography-Mass Spectrometry (GC/MS). 34 components were identified, accounting 59.4% of the total oil, which (Z)-heptadeca-10,16-dien-7-one (ZHD) was the major component with 28 % of the oil. The protective effect of this oil on the corrosion of mild steel (MS) in 1M HCl solution was tested by the measurements of Weight loss (WL), potentiodynamic polarization (PDP), electrochemical impedance spectroscopy (EIS). From WL measurements, the inhibiting effect was raised with the increasing of both concentration inhibitor and temperature. PDP curves led to a mixed-type inhibitor. The charge transfer process mainly controls the results of EIS measurements. The SP oil adsorption not only was discovered to obey Langmuir isotherm but showed a chemical interaction as well. The computational methods such as density functional theory (DFT), Monte Carlo (MC) and radial distribution function (RDF) simulations were also performed to analyze the possible contribution of (Z)-heptadeca-10,16-dien-7-one (ZHD) to the corrosion prevention effect of global oil.

Keywords: Santolina pectinata Lag, Essential oil, (Z)-heptadeca-10,16-dien-7-one, Mild steel; Corrosion.

1. Introduction

In the broad spectrum of industries, MS tendency to corrosion is caused by aggressive acids such as hydrochloric and sulphuric acids, which are widely used in the pickling processes of metals ^{1,2}. Therefore, tremendous efforts are being made in order to block or delay the attack of this metal in numerous corrosive media. The use of corrosion inhibitors is viewed as the best way to prevent the corrosion of metal surfaces ³. Almost all inhibitors of corrosion are synthetic

organic compounds ⁴. Owing to the high cost, toxicity, and dangerous effects of synthesized corrosion inhibitor ^{5, 6}, the search for green alternatives that are eco-friendly and non-toxic to protect health and ensure human security is at present attractive ⁷⁻¹³. In our laboratory, a great deal of research has been carried out to study inhibitive effect using plant extract on the corrosion of steel in acidic media. ¹⁴⁻¹⁹. In this study, our focus is chiefly put on the essential oil of *Santolina pectinata (Lag.)* (Figure 1).

Santolina pectinata Lag. is, Botanically, a synonym of Santolina rosmarinifolia subsp. pectinata Lag. Maire. It is an endemic herbaceous medicinal, aromatic plant originating from North Mediterranean, mainly found in the Iberian System, North Africa and principally in the eastern Baltic mountains²⁰. In Morocco, this species, known locally as "tayrart", is a natural plant which often grows, frequently with Cedrus atlantica and Abie spinsapo, on calcareous substrates in 1500 m above sea level. On the other hand, it is associated with Quercus ilex and Q. canariensis at lower levels ²¹. S. pectinata Lag.is an infrequently studied Iberian-Maghreb endemic and, to our knowledge, only one study has investigated the chemical composition of essential oil of this plant collected at Pontones (Jakn) from Spain²². The phytochemical analysis and biological characteristics of Santolina species from various origins have also been widely dealt with ²³. Previous studies have shed in evidence the presence of terpenoids, such as germacrane sesquiterpenoids, chrysanthemane monoterpenoids eudesmane,

flavonoids and coumarins and other secondary metabolites ²⁴⁻²⁷.



Figure 1. Santolina pectinata (Lag.) in its native habitat in south-eastern of Morocco

Many Santolina species have been used in traditional medicine for a long time ^{23,28, 29}. The main objective of the current research is to study the preventive impact of SP oil as a substance naturally acting on corrosion behavior of MS in 1M HCl solution. ZHD is quite likely the major active ingredient which is responsible for the corrosion inhibition of SP oil. To demonstrate that ZHD is really responsible for the anticorrosion effect, this molecule is isolated by fractionation of essential oil using successive column chromatography. After that, a comparative study of SP oil and ZHD alone is carried out. More than that, so as to clarify the interactions between ZHD and the surface of the iron metal, computational calculations based on DFT, Parr functions analysis, MC and RDF simulations were also performed.

2. Experimental details

2.1. Inhibitors

The experimental phase followed in the current study such as extraction of SP oil, oil fractionation and isolation of ZHD, GC-MS and NMR analysis have been mentioned according to a formerly described experimental procedure in our work ³⁰. The concentration range of SP oil was 0.25-3 g/L in acidic media.

2.2. Corrosion test

2.2.1 Preparation of materials

MS (2 cm×2 cm) coupons containing 0.09 wt.% (P), 0.38 wt.% (Si), 0.01 wt.% (Al), 0.05 wt.% (Mn), 0.21 wt.% (C), 0.05 wt.% (S) and the remainder iron (Fe) were used to measure weight loss. The corrosive medium is 1 M HCl was prepared by dilution of HCl (37%) with distilled water.

2.2.2 Weight loss measurements

The specimens of steel were meticulously washed in double-distilled water, dried and then weighed after 6 hours of immersion (100 ml corrosive solution). Weight loss enabled us to calculate the mean corrosion rate as expressed in mg.cm⁻² h^{-1} . The corrosion rate (Wcorr) and also the inhibition

effectiveness Ew (%) were calculated based on the Eqs. (1) and (2) respectively:

$$W = \frac{\Delta m}{S.t}$$
(1)

$$E_{w} \% = \frac{W_{corr} - W_{corr(inh)}}{W_{corr}} \times 100$$
(2)

where Δm (mg) is the specimen weight before and after immersion in the tested solution, Wcorr and Wcorr(inh) are the values of corrosion weight losses (mg/cm².h) of MS in uninhibited and inhibited solutions, respectively, S is the area of the mild steel specimen (cm²) and t is the exposure time (h). The degree of surface coverage was calculated using:

$$\theta = \frac{W_{\text{corr}} - W_{\text{corr}(\text{inh})}}{W_{\text{corr}}}$$
(3)

Where θ is surface coverage; Wcorr (inh) is corrosion rate for steel in the presence of inhibitor, Wcorr is corrosion rate for steel in the absence of inhibitor.

2.2.3 Electrochemical studies

Electrochemical measurements were conducted in a conventional three-electrode electrolysis cylindrical Pyrex glass cell. The working electrode (WE) in the form of disc cut from steel has a geometric area of 1 cm² and is embedded in polytetrafluoroethylene (PTFE). A saturated Ag/AgCl electrode and a disc platinum electrode were used respectively as reference (RE) and counter electrodes (CE).

The corrosion inhibition efficiency was derived as given below:

$$E_{i}(\%) = \left(\frac{I_{corr} - I_{corr,inh}}{I_{corr}}\right) \times 100$$
(4)

Where I_{corr} , $I_{\text{corr,inh}}$ and represent the corrosion current densities not including and by way of the existence of inhibitor.

Electrochemical impedance spectroscopy measurements were achieved at the open circuit potential for the frequency range of 100 KHz to 10 mHz, using a peak-to-peak voltage excitation of 10 mV.

The inhibition efficiency $E_{Rt}(\%)$ was calculated from R_t using the following equation:

$$E_{Rt}(\%) = \left(\frac{R'_t - R_t}{R'_t}\right) \times 100$$
(5)

Where R_t and R'_t are the charge-transfer resistance values without and with inhibitor respectively. R_t is the diameter of the loop.

The double-layer capacitance (C_{dl}) and the frequency at which the imaginary component of the impedance is maximal (-Zmax) are found determined by Eq. (6):

$$C_{dl} = \frac{1}{\omega R_{t}}$$
(6)

where $\omega = 2\pi$. f_{max}

Impedance diagrams are obtained for the frequency range 100 KHz–10 mHz at the open circuit potential for MS steel in 1 M HCl in the presence and absence of SP oil.

2.3. Computational details

The optimized geometry of the major extract component was performed utilizing DFT method ³¹ using program Gaussian 09 ³² in the scheme of B3LYP hybrid functional ³³ with the 6-311G++(d,p) basis set ³⁴. Then, the local electrophilic, P⁺, and nucleophilic, P⁻, Parr functions ³⁵ are obtained from the analysis of the Mulliken atomic spin density (ASD) at the radical anion and at the radical cation by adding and removing an electron to the studied inhibitor, respectively. Concerning MC and RDF simulations ^{36,37}, the iron surface (111) is built-in Biovia Materials studio 8.0 ³⁸ as follows: slab thickness of 45 Å, a supercell of (7*7) and a vacuum of 30 Å along the ox, oy and oz axis in a simulation

box Fe(111) (i.e., Lx=Ly=Lz= 30 Å) with periodic boundary conditions to model a representative part of the interface without any arbitrary boundary effects. The build surface of Fe (111) is optimized using Materials studio DMol^{^3} at the DNP+ basis and B3LYP functional. Besides, the complete MC simulation goals to study alignment and adsorption behavior in two environments: at first, in a vacuum (one molecule of ZHD and Fe(111) surface) and secondly, in solution (one molecule of ZHD, 10 entities of oxonium ions (H₃O⁺), 15 molecules of water and Fe(111) surface) using COMPASS II force field ³⁹ by means the adsorption locator module integrating in Biovia Materials studio version 8.0. The adsorption behavior was evaluated through RDF analysis using Forcite calculation code ⁴⁰. The intense peak happened from 1 Å up to 3.5 Å, which is considered a sign of small bond length, which correlates to chemical adsorption. The physical adsorption, on the other hand, is associated with the intense peak that is longer than 3.5 Å 41,42 .

3. Results and discussion

3.1. Essential oil composition

The use of CC, GC-RI, GC-MS, ESI (+)-MS, 1D and 2D-NMR analyses contributed to the identification of SP oil. Then, 34 components were identified, accounting 59.4% of the total amount. The SP oil was dominated by oxygenated compounds (47.9%) while hydrocarbon compounds didn't exceed 11.5% of the oil. A non-terpenic oxygenated compound *i.e.*, (Z)-heptadeca-10,16-dien-7-one (ZHD) was the major component with 28% of the oil (Table 1 and Figure 2)³⁰.

Table 1. Chemical composition of S. pectinata Lag. aerial parts essential oil.

N ^a	Components ^b	Ir Lit ^c	Ir apo ^d	Ir pol ^e	0∕0 ^f
1	Cineole 1,8	1024	1019	1206	0.1
2	Limonene	1024	1021	1199	0.2
3	(Z)-b-Ocimene	1029	1025	1231	1.6
4	(E)-b-Ocimene	1041	1036	1247	0.1
5	Nonanal	1076	1081	1394	0.1
6	Linalool	1086	1083	1544	0.2
7	Cis Sabinene hydrate	1083	1097	1553	0.4
8	β-Thujone	1103	1107	1422	0.4
9	Camphor	1123	1121	1519	0.5
10	Lyratol	1150	1138	1779	0.4
11	Borneol	1150	1149	1689	0.3
12	α-Terpineol	1176	1172	1684	0.2
13	Estragole	1175	1175	1661	0.5
14	Cuminaldehyde	1217	1212	1779	0.9
15	p-Anisaldehyde p	1215	1214	2028	0.6

	Others				6.6	
Nonterpenic oxygenated compounds						
Oxygenated sesquiterpenes						
Hydrocarbon sesquiterpenes						
	Oxygenated mor	noterpenes			6.8	
	Hydrocarbon mo	noterpenes			1.9	
	Total ident	tified			59.4	
34	(Z)-heptadeca-10,16-dien-7-one		1834	2242	28	
33	Tau cadinol	1633	1625	2154	1.3	
32	Dillapiole	1590	1591	2338	1.2	
31	Caryophyllene oxyde	1578	1570	1967	3.4	
30	Spathulenol	1572	1564	2105	1.1	
29	Germacrene D	1479	1475	1701	1.3	
28	α-Curcumene	1473	1470	1765	0.3	
27	E-β-Farnesene	1446	1447	1661	1.2	
26	E-Caryophyllene	1421	1416	1593	6	
25	Isocaryophyllene	1409	1403	1570	0.2	
24	Methyleugenol	1369	1374	2000	0.2	
23	α-Copaene	1379	1371	1489	0.6	
22	Carvacrol	1278	1278	2214	0.6	
21	Undecan-2-one	1273	1272	1586	0.6	
20	Thymol	1266	120)	2190	0.0	
19	Bornyl acetate	1202	1269	1573	0.8	
18	E-Anethole	1270	1263	1813	4.1	
16 17	Peryllaldehyde Lyratyl acetate	1248 1270	1248 1257	1768 1634	1.6 0.2	

^a Order of elution is given on apolar coloumn (Rtx-1)

^b Normalized % abundances of oil are given on the apolar column

^c Retention indices from the literature on the apolar column

^d Retention indices on the Rtx-1 apolar column

^e Retention indices on the Rtx-wax polar column

^f Percentage composition is given on the apolar column

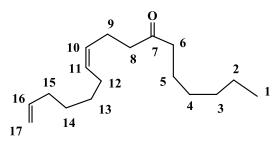


Figure 2. Chemical molecular structure of ZHD

3.2. Corrosion tests3.2.1. Effect of temperature

In this paragraph, we determine the WL of the MS sample in corrosive solution with and without

different concentrations of SP oil at different temperatures (308-343K). The values of percentage

inhibition efficiency E_w (%) and the corrosion rate (W) obtained are summarized in Table 2.

Table 2. Weight loss results for MS in 1 M HCl with and without different concentrations of aqueous extract at different temperatures.

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C (g/L)	308 K		313 K		323 K		333 K		343 K	
	W (mg/cm²h)	Ew (%)	W (mg/cm ² h)	Ew (%)	W (mg/cm ² h)	Ew (%)	W (mg/cm ² h)	E _w (%)	W (mg/cm ² h)	E _w (%)
0.00	0.942		1.751		2.836		3.641		6.301	
0.25	0.254	73.03	0.420	76.01	0.637	77.54	0.813	77.67	1.401	77.76
0.50	0.194	79.4	0.344	80.35	0.554	80.46	0.700	80.77	1.200	80.95
1.00	0.150	84.07	0.245	86.00	0.369	86.98	0.441	87.88	0.687	89.09
2.00	0.131	86.09	0.221	87.37	0.338	88.08	0.373	89.75	0.598	90.51
3.00	0.096	89.8	0.155	91.14	0.230	91.88	0.257	92.94	0.399	93.66

The results (Table 2) show that inhibitive efficiency E_w (%) goes up considerably with the increase in the concentration of SP oil, indicating that the extent of inhibition depends on the concentration of this inhibitor.

Besides, we notice that these findings demonstrate that the effectiveness of E_w (%) depends on the temperature and increases when it rises from 308 to 343 K. More than that, when the concentration reached to 3 g/L, the effectiveness (E_w) reached a high value of 93.66 % in 1 M HCl solution at 343 K. This

increase can be attributed to the strong adsorption of SP oil resulting in the formation of a protective layer on the steel surface.

3.2.2. Polarization tests

The PDP curves of MS in 1 M HCl solution without and with a concentration of SP oil at 308 K are shown in Figure 3. Current density (I_{corr}), corrosion potential (E_{corr}), cathodic and anodic Tafel slopes (βc , βa) are the polarization parameters. These parameters and inhibition efficiency (E_i%) are calculated from the Tafel curves and are summed up in Table 3.

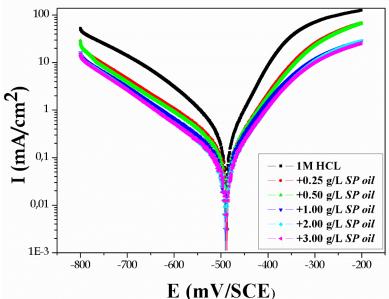


Figure 3. Polarization curves of MS in 1 M HCL with and without SP oil at various concentrations at 308 K

It is obvious from Figure 3 that the fact of adding SP oil has an inhibitive effect in both the anodic and cathodic parts of the polarization curves. This reveals a modification of the mechanism of cathodic hydrogen evolution and also the anodic dissolution of

steel. This, of course, indicates that inhibitor considerably blocks the corrosion process of MS thanks to the adsorption of an organic compound (heteroatom such as oxygen) 43 .

Table 3. Electrochemical parameters for MS in 1 M HCl containing different concentrations of SP oil at 308K.

C (g/L) - E _{corr} (mV SCE) I _{corr} (mA cm ²) -βc (mV) βa (mV) Ei%

0	490.1	0.5779	147.4	74.8	
0.25	480.0	0.2214	163.0	57.0	62.00
0.50	480.0	0.1840	159.2	54.0	68.16
1.00	490.0	0.1243	150.6	52.1	78.50
2.00	490.0	0.0907	142.6	42.0	84.50
3.00	480.0	0.0865	143.2	43.1	85.03

Examination of the data in Table 3 shows that the corrosion current densities (I_{corr}) go down significantly with the increase of SP oil concentration. Correspondingly, the inhibition efficiency $(E_i\%)$, goes up with the inhibitor concentration to reach its maximum value, 85.03 %, at 3 g/L. This behavior

reveals that the SP oil diminishes the corrosion of MS in HCl solution and behave as a mixed type ⁴⁴.

3.2.3. Electrochemical impedance spectroscopy (EIS)

Nyquist plots of steel in 1M HCl at various concentrations of this oil are given in Figure 4.

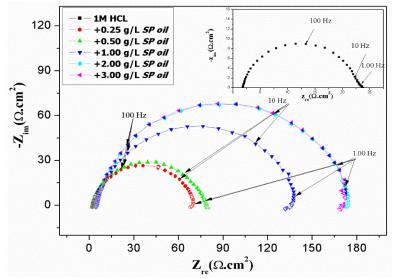


Figure 4. Nyquist plots of MS in 1 M HCL containing various concentrations of SP oil

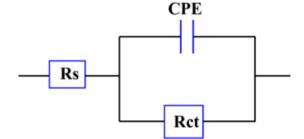


Figure 5. The equivalent circuit used to fit the EIS experiment data

The addition of the SP oil (0.25-3g/L) studied to the corrosive solution leads to an increase in the diameter of the depressed semicircular form. The diameter of Nyquist plots rises with increasing inhibitor concentration. The latter asserts the adsorption of the inhibitor on the metal surface.

Moreover, the impedance spectra present one single capacitive loop, which indicates that the charge transfer takes place at the electrode/solution interface ⁴⁵. What is more, is that these capacitive loops are not the perfect semicircles because of a common dispersion effect ⁴⁶. that has been attributed to roughness and other inhomogeneities of solid surface ⁴⁷.

 Table 4. Characteristic parameters evaluated from the impedance diagram for MS in 1 M HCl at various concentrations of SP oil.

C (g/L)	$R_{ct} (\Omega \ cm^2)$	f max(Hz)	Cdl (µF cm ²)	E _{Rt} %
0.00	21.69	100	73.37	
0.25	067.2	50	47.35	67.73
0.50	078.6	50	40.51	72.39
1.00	126.8	31	39.67	82.98
2.00	166.2	31	38.30	86.95
3.00	169.4	31	37.58	87.19

We can conclude from the data obtained about impedance (Table 4) that the R_{ct} values go up as a result of inhibitor concentration and in consequence, the E_{Rt} goes up to reach the highest value 87.19% at 3 g/L. On the other hand, the decrease in C_{dl} is caused by the adsorption of the inhibitor on the metal surface, leading to the formation of film or complex from acidic solution ⁴⁸. Addition of SP oil resulted in lower C_{dl} values, probably because of the substitute of water molecules by the inhibitor molecules at the electrode surface. The (EIS) results of these capacitive loops are simulated by the equivalent circuit shown in Figure 5 ⁴⁹. In the equivalent circuit, R_s is the electrolyte resistance, R_{ct} the charge transfer resistance and C_{dl} is the double layer capacitance ⁵⁰.

3.3. Kinetic/Activation parameters

The following study consists of calculating activation parameters of the corrosion reaction such as activation energy E°a activated entropy Δ S°a and activation enthalpy Δ H°a were calculated using the Arrhenius, and its alternative formulation called transition state Eqs 7 and 8 ⁵⁰.

where E°a is the apparent activation corrosion energy, T is the absolute temperature, R is the universal gas constant, A is the Arrhenius pre-exponential factor, h is the Plank's constant. N is the Avogadro's number, Δ S°a is the entropy of activation and Δ H°a is the enthalpy of activation.

The activation energies are inferred from the slope (-E°a/R) of the logarithm of the corrosion rate (W) versus reciprocal absolute temperature (Figure 6). Their values were reported in Table 5. Using more Eq. (8) plots of Ln (W/T) versus 10³/T (Figure 7) result in straight lines with a slope of (- Δ H°a/R) and an intercept of (Ln(R/Nh) + (Δ S°a/R)) from which the values of Δ H°a and Δ S°a were calculated and are listed in Table 5.

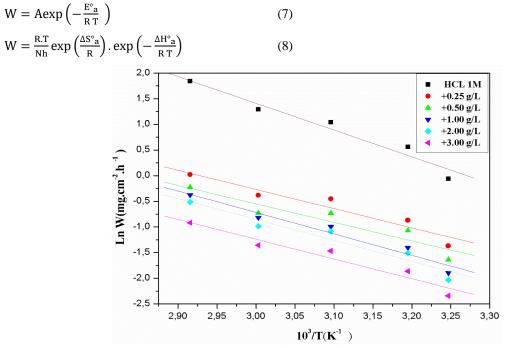


Figure 6. Arrhenius plots for MS corrosion rates (W) in 1M HCl in the absence and presence of different concentrations of SP oil

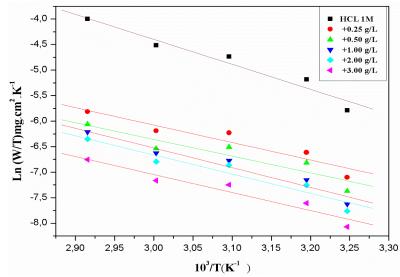


Figure 7. Transition-state plot for MS corrosion rates (W) in 1 M HCl in the absence and presence of various concentrations of SP oil

Table 5. Calculated values of kinetic parameters for MS corrosion in 1 M HCl solution in the absence and presence of various concentrations of SP oil.

C (g/L)	E°a(kJ mol ⁻¹)	$\Delta H^{\circ}_{a}(kJ mol^{-1})$	$E_{a-}\Delta H^_a(kJmol^{-1})$	$\Delta S^{\circ}_{a}(J \ mol^{-1} \ K^{-1})$
HCl 1M	43.35	40.65	2.70	-112.32
0.25	31.14	28.44	2.70	-162.93
0.50	29.97	27.27	2.70	-168.77
1.00	34.75	32.05	2.70	-155.85
2.00	33.91	31.21	2.70	-159.47
3.00	32.02	29.32	2.70	-168.36

The activation energies in the presence of SP oil are lesser to those in uninhibited acid solution (Table 5). So, the addition of SP oil decreases metal dissolved in 1M HCl medium. We note that the increase of E_w (%) and the lower value of $E^{\circ}a$ are in favor of chemisorption ⁵¹. The positive value of enthalpy of activation ($\Delta H^{\circ}a$) in the presence of various concentrations of inhibitor shows the endothermic nature of the MS dissolution process, implying that dissolution of steel becomes difficult ⁵². However, the negative values of entropy of $activation(\Delta S^{\circ}a)$ indicate that a decrease in disordering takes place continuously from reactants to the activated complex. The activated complex in the rate-determining step represents an association rather than a dissociation step ⁵³. On the other hand, the average difference value of the $E^{\circ}a-\Delta H^{\circ}a$ is 2.7 KJ.mol⁻¹, which is almost equal to the average value of RT (2.7 KJ.mol⁻¹) at the average temperature (323 K) of the domain in question. This result agrees that the corrosion process is a unimolecular reaction as described by the known Eq. (9) of perfect gas:

$$\mathbf{E}^{\circ}\mathbf{a} - \Delta \mathbf{H}^{\circ}\mathbf{a} = \mathbf{R}\mathbf{T} \tag{9}$$

3.4. Adsorption isotherm and thermodynamic parameters

In this work, we evaluated several types of adsorption isotherm (Frumkin, Temkin and Langmuir). Langmuir was found to give the best description on the adsorption of SP oil. Figure 8 reflects a straight line ($\mathbb{R}^2 \approx 1$) by plotting C/ θ with regard to the concentration and the corresponding equation. (Eq. (10)) is as follows: Adsorption constant (K_{ads}) value was demonstrated by the intersection of the obtained straight curve and C/ θ axis (Table 6):

$$\frac{C}{\theta} = \frac{1}{K_{ads}} + C \tag{10}$$

The equilibrium adsorption constant, K_{ads} is connected to the standard Gibb's free energy of adsorption (ΔG°_{ads}) with the following equation ⁵⁴:

$$K_{ads} = \frac{1}{55.5} \exp\left(-\frac{\Delta G^{\circ} ads}{RT}\right)$$
(11)

where R, T, 55.5 are gas constant, absolute temperature of experiment the molar concentration of water in solution in respectively.

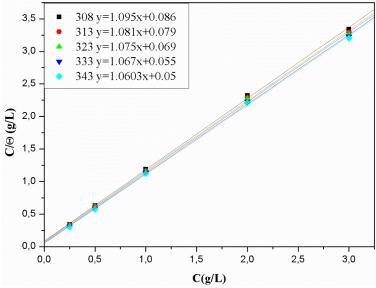


Figure 8. The Langmuir adsorption isotherm of SP oil on the MS surface in 1 M HCl at different temperatures

Table 6. Thermodynamic parameters for adsorption of SP oil on MS in 1M HCl solution at different temperature	s
from Langmuir adsorption isotherm.	

T(K)	R ²	Kads (L g ⁻¹)	ΔG° ads (kJ mol ⁻¹)
308	0.999	11.52	-23.96
313	0.999	12.61	-24.59
323	0.999	14.37	-25.72
333	0.999	18.11	-27.16
343	0.999	20.04	-28.27

Data in Table 6 revealed that the SP oil was quickly and strongly adsorbed onto the MS surface at a relatively higher temperature. This could be due to the creation of a coordinated bond between the SP oil molecules and the d-orbital of iron ⁵⁵. Here, the calculated ΔG^0 ads values are ranging from -23,96 to -28,27 kJ.mol⁻¹, showing that the adsorption mechanism of SP oil on MS in 1 M HCl solution at the studied temperatures may be a combination of both electrostatic-adsorption and chemisorption ⁵⁶.

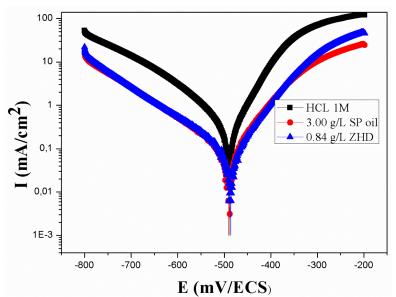


Figure 9. Comparison of polarization curves for MS in 1M HCl containing 3 g/L of SP oil and 0.84 g/L of ZHD

3.5 Constituent responsible for inhibition

The results undoubtedly demonstrated that the inhibitor molecules inhibit the corrosion of the steel surface.

As a consequence, compared together, both SP oil and ZHD are the principal constituents to confirm that this latter is responsible for corrosion inhibition properties of the total oil. In this sense, the ZHD is isolated and evaluated electrochemically by PDP and EIS measurements. Electrochemical test solutions were prepared using a concentration of 3 g/L of SP oil and 0.84 g/L (28% of 3 g/L) of ZHD molecules. We present in Figure 9 the PDP curves of MS in 1 M HCl solution with and without a concentration of 3 g/L of SP oil and 0.84 g/L of ZHD. current density (I_{corr}), corrosion potential (E_{corr}), cathodic and anodic Tafel slopes (β_c , β_a) are the polarization parameters. The parameters and percentage inhibition efficiency (E_i%) are calculated based on the Tafel curves and are given in Table 7.

Table 7. Polarization parameters and the corresponding inhibition efficiency for the corrosion of MS in 1M HCl containing 3 g/L of SP oil and 0.84 g/L of ZHD at 308 K.

	C (g/L)	- E _{corr} (mV SCE)	I _{corr} (mA cm ²)	-βc (mV)	βa(mV)	E _i %
HCl 1M	0.00	490.0	0.5779	147.4	74.8	
SP oil	3.00	480.0	0.0865	143.2	43.1	85.03
ZHD	0.84	490.0	0.0848	140.7	40.3	85.33

According to Figure 9, the presence of ZHD causes a prominent decrease of current densities for anodic and cathodic Tafel curves. This decrease indicates the inhibition of anodic metal dissolution and the cathodic hydrogen evolution reaction. This behavior reveals that the ZHD reduces the corrosion of MS in HCl medium and acts as a mixed type.

of 85.03% and 85.33% at concentration of 3 g/L and 0.84 g/L, respectively. These results indicate that the ZHD molecule can be determined as being the constituent responsible for the inhibitive action of SP oil. The Nyquist plots of steel in 1 M HCl containing 3 g/L of SP oil and 0.84 g/L of ZHD are shown in Figure 10. As for the impedance data, they are given in Table 8.

It is crystal clear from the data in Table 7 (attested) that the SP oil and ZHD show a protective efficiency

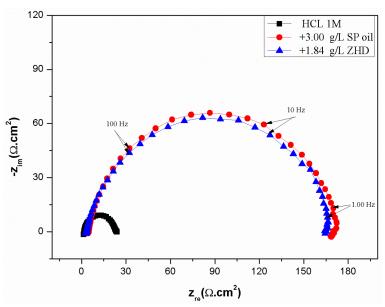


Figure 10. Comparison of Nyquist plots for MS in 1MHCl containing 3 g/L of SP oil and 0.84 g/L of ZHD molecules

The impedance spectra present one single capacitive loop, indicating that the charge transfer takes place at the electrode/solution interface and the size of the capacitive loop is similar for the SP oil and the ZHD. The presence of the maximum concentrations of inhibitors augments the value of R_t in acidic solution. The impedance data in Table 8 indicates that the R_t goes up, and the C_{dl} goes down because of a decrease in local dielectric constant and/or an increase in the thickness of the electrical double layer. Therefore, the inhibition efficiency (E_{Rt}) increases to 87.19 and 87.81 % at 3 g/L for SP oil and 0.84 g/L for ZHD, respectively. The inhibition efficiencies provided by ZHD molecule and SP oil are practically similar. These results assert again that the ZHD molecule can be determined as being the component responsible for the inhibitive effect of SP oil.

	C (g/L)	-E _{corr} (mV SCE)	$R_t (\Omega \ cm^2)$	$f_{max}(H_Z)$	$C_{dl}(\mu F \ cm^{-2})$	E _{Rt} %
HCl 1M	0.00	490.1	21.69	100	73.37	
SP oil	3.00	480.0	169.4	31	37.58	87.19
ZHD	0.84	490.0	171.0	25	37.22	87.31

Table 8. Characteristic parameters evaluated from the impedance diagram for MS in 1 M HCl containing 3 g/L of SP oil and 0.84 g/L of ZHD at 308K.

3.6. Theoretical study of reactivity and adsorption behaviors

The optimized geometry illustrated in Figure 11 of the inhibitor (Z) -heptadeca-10,16-dien-7-one designed (ZHD) was confirmed by the presence of one and only imaginary frequency in the hessian matrix. The quantum parameters such as the energy of the highest occupied molecular orbital (E_{HOMO}), electronic chemical potential, μ , chemical hardness η_{inh} , the energy of the lowest unoccupied molecular orbital (E_{LUMO}), fraction transferred electron between the inhibitor and iron metal, ΔN , electronegativity, χ and

dipole moment were calculated ³¹ (Table 9). These parameters are shown as follows:

$$\mu = -\chi = \frac{E_{HOMO} - E_{LUMO}}{2}$$
(12)

$$\eta_{inh} = E_{LUMO} - E_{HOMO}$$
(13)

$$\Delta N = \frac{\chi_{Fe} - \chi_{inh}}{2(\eta_{Fe} + \eta_{inh})}$$
(14)

In this research, we use the theoretical value of $\chi_{Fe} = 7.0 \text{ eV}$ and $\eta_{Fe} = 0 \text{ eV}$ on the assumption that (for) a metallic bulk ionization potential (I) is equal to an electron affinity (A) as they are softer than the neutral metallic atoms ⁵⁷.

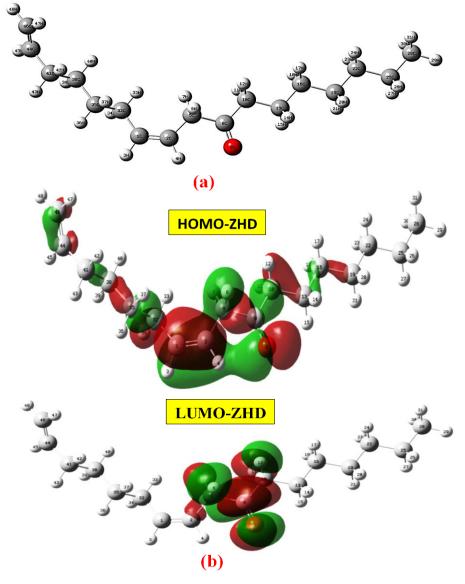


Figure 11. (a) Optimized structure of ZHD (b) HOMO and LUMO plots of ZHD

Table 9. Quantum chemical parameters for ZHD. E_{HOMO} and E_{LUMO} (in eV), electronic chemical potential μ (in eV), chemical hardness η (in eV), electronegativity χ (in eV), the fraction of transferred electrons ΔN and dipole moment (in Debye) calculated using 6-311G++(d,p) in the gas phase.

Еномо	Elumo	μ	η_{inh}	X	$\Delta \mathbf{N}$	Dipole moment
-6.53	-0.46	-3.04	6.07	3.04	0.33	3.33

From Table 9, the electronic chemical potential of ZHD (-3.04 eV) is higher than of iron metal (-7.00 eV). It indicates that the ZHD molecule has the strongest electron-donating ability to the iron metal. This result showed that the inhibitor molecule can give electrons to the empty 3d orbital of iron metal, forming a coordinate bond. Therefore, it appears that the fraction transferred electron is positively and less than 3.6 ($\Delta N = 0.33$), revealing obviously that inhibition efficiency is only remaining to the electrondonating capability of the inhibitor ⁵⁷. Besides, the dipole moment of inhibitor (3.33 Debye) is higher than of water (2.16 Debye) indicating that this inhibitor has superior affinity to interact with metal as compared to the water. It means that the natural compound can adsorb on the MS surface by replacing the adsorbed water molecules.

Nucleophilic and electrophilic sites of the inhibitor structure were examined by the nucleophilic P- and

electrophilic P+ Parr functions, respectively (Table 10). Analysis of the nucleophilic P- Parr of ZHD demonstrates that the reactive atoms (largest values of P-) are located over the carbonyl C=O both ethylenic group and bond (C1=C2 and C44=C46). For example, the most reactive ones for ZHD are oxygen atom O9 and carbon atoms C1, C2, C44 and C46. Consequently, these centers will interact healthily around the iron surface (110). In other words, the values of electrophilic P⁺ Parr function indicate that the most electrophilic atoms are as follows: C1, H6, C25, C44 and H45 (highest values of P⁺). Based on these results, we can deduce that the studied inhibitor which can donate electrons to unoccupied d orbital of the iron surface to form coordinate covalent bonds and can also accept free electrons from the iron surface by using their anti-bonding orbital to form feedback bonds.

Atoms	P-	Atoms	P+
1 C	0.174	1 C	0.996
2 C	0.136	2 C	-0.354
5 C	0.026	3 H	0.135
6 H	0.021	5 C	0.211
9 O	0.215	6 H	0.537
10 C	0.070	12 H	0.359
13 C	0.010	17 H	0.198
16 C	0.016	18 H	0.110
19 C	0.014	25 C	0.682
22 C	0.009	26 H	0.105
25 C	0.007	29 H	0.395
28 C	0.004	30 H	0.226
38 C	0.013	31 H	0.229
41 C	0.008	33 H	0.168
44 C	0.098	34 H	0.201
46 C	0.179	44 C	1.166
****	****	45 H	0.542
****	****	47 H	0.231

Table 10. Nucleophilic P- and electrophilic P+ Parr functions of inhibitor ZHD.

The most stable configuration of adsorbate/Fe (111) surface system was obtained in both phases vacuum and solution using the adsorption locator module of

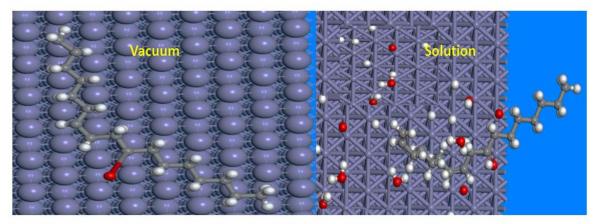
MC simulation. In fact, different energies were calculated such as the adsorption energy $(E_{ads})^{42}$, the rigid adsorption energy $(E_{Rads})^{42}$, the deformation

energy $(E_{Def})^{42}$ and the compulsory energy to exclude inhibitor from the iron surface $(dE_{ads}/dNi)^{42}$ (Table 11). A bright idea about the most stable adsorption configuration and Radial distribution

function RDF (or pair correlation function g(r)) in a vacuum and in solution are shown in Figure 12.

Table 11. Adsorption energy E_{ads} , rigid adsorption E_{Rads} , deformation energy E_{def} and necessary energy to exclude inhibitor from the iron surface dE_{ads}/dNi , in kcal/mol, are given in vacuum and solution.

	$\mathbf{E}_{\mathrm{ads}}$	E _{Rads}	$\mathbf{E}_{\mathbf{Def}}$	dEads/dN (ZHD)
Vacuum ZHD/Fe(111)-surface	-42.38	-176.08	-38.77	-42.38
Solution ZHD/15H2O/10H3O ⁺ /Fe(111)-surface	-563.97	-22.12	-563.97	-28.17



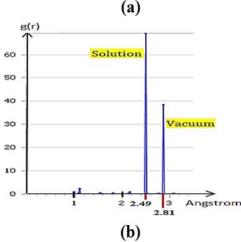


Figure 12. (a) Top view of the most stable adsorption configuration for the adsorption of the studied molecule on Fe (111). (b) Radial distribution function RDF (g(r)).

The negative values of the adsorption energies for both phases, pointing out that the interaction between inhibitor molecule and Fe (111) surface is a spontaneous process. Besides, the lower adsorption energy in the solution is a sign of a high inhibition effect in this medium. As such, energy deformation goes down following the order: E_{Def} (solution) < E_{Def} (vacuum) points to a strong adsorption behavior in the solution than in the vacuum. This result is, to a large extent, consistent with the experiment.

From Figure 12(a), it is made crystal clear that the inhibitor is adsorbed on Fe (111) surface in a parallel form with close contact of Fe atoms. This can be explained by the strong interaction of the reactive sites of inhibitor with the metal surface as already discussed. Consequently, the inhibitor can be

adsorbed on the iron surface through not only on the oxygen atom but also over the unsaturated hydrocarbon regions (C1=C2 and C44=C46). This result presents the similarity with that deduced from nucleophilic P– Parr function.

Radial distribution function RDF (or pair correlation function g(r)) analysis is considered to be of great importance to estimate the bond length and consequently the molecule surface interaction modes (Figure 12 b). As a consequence, the adsorption process of the studied system is the chemisorption type. This is (in) consistent with the present experiment. Also, through this analysis, we noticed that the finding length that is between the iron surface and adsorbent is decreased in case of the solution medium; indicates that the adsorption efficiency would be more in the solution than in the vacuum.

4. Conclusion

All in all, The SP oil has proved to be able to inhibit MS corrosion in 1M HCl solution efficiently. The charge transfer resistance (R_t) increases and the double-layer capacitance (C_{dl}) decreases due to adsorption of the SP oil on the surface of MS. The natural oil acts on MS surface in 1 M HCl solution as mixed-type inhibitor. The adsorption of the SP oil not only was found to obey Langmuir isotherm but also showed a chemical interaction. We can conclude that the natural substance ZHD from SP oil is responsible for corrosion inhibition and that the Quantum chemical calculations by DFT calculations and Monte Carlo simulation are coherent with the experimental findings.

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